Design of PLC control system



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Background of Project

Methodology

Abstract

This project, involves the design of two water tank processes that work in tandem with a Siemens 1200 PLC system to offer a control framework for the process that maintains water level and temperature in the specified water tanks at a set point.

Below picture shows a P&ID diagram of the Rig which can be seen in figure 3. The blue tint represents the flow of water in the tank as it passes through the pipes. A ultrasonic level sensor can be seen detecting the process variable, which in this case is the liquid level in tank B102, the higher tank. The system's pump, designated P101, serves as an actuator, while the lower tank, designated B101, serves as a reservoir.[1]



PID Control

PID (Proportional-Integrative-Derivative) controllers are employed in almost every industrial control environment across the world. They have a simple design with only three parameters, which is part of the reason for their success; they are simple and straightforward to operate. This is the most popular choice among control engineers because the simple design is much easier to apply to control systems than more complicated control techniques





Project requirements



- Review the Siemens PLC 1200 and study the best practice regarding interfacing sensors and components with the platform.
- Investigate, prescribe, deploy and test a control strategy for the system.
- Design and build a user-friendly interface to control the sensors of the system.
- Critically analyse the performance of the system.



Sensor	<	

Tuning a PID controller

Any project that uses a controller must be tailored to a specific environment. This entails deciding which control modes to utilize and which control settings to use. This means determining whether proportional control, proportional plus derivative, proportional plus integral or proportional plus integral plus derivative is to be used and selecting the values of KP, KI and KD These influence how the system reacts to a disturbance or change in the set value, how quickly it responds to changes, how long it takes to settle down after a disturbance or change in the set value, and whether a steady state error will occur. [2]

$$u(t) = K_p e(t) + K_i \int_0^t e(t)dt + K_d \frac{de(t)}{dt}$$

- \succ u(t) = PID control variable.
- \succ K_P = Gain (Proportional). This is a linear response to the error.
- \blacktriangleright e(t) = error value
- \succ K_I = Reset (Integral). Elimination of the offset error introduced by linear response.
- \blacktriangleright de = change in error value
- \blacktriangleright dt = change in time

Results				
Disturbance 100%	Disturbance 50%	Control of level attained with	Conclusions	
➤ Below shows the flow rate when the disturbance value has been opened	► Below shows the flow rate when the disturbance value is opened by 50%	Transfer function.	► Level was controlled using a PI	
100%.	The issue of the isopened by 50%.	\succ The tuned level was attained using PI		

 \succ This is the outlet flow of water with no pump running and the disturbance valve been fully open.

Flow Rate Out 100%

140

120

80

Ê 100

 \succ This is the outflow of water with a 50% disturbance in the system.

120

100

80

60

y = -1.2946x + 110.21

 $R^2 = 0.9414$

 \succ The PI controller counteracted this outflow with the Pump and maintained level with minimal error.

y = -0.7748x + 103.13

 $R^2 = 0.9751$

Flow Rate Out 50%

- control.
- Constants used for tuning were a gain of 17, and integral of 2 seconds.

Level with PI Control

- System is a first order response.
- \triangleright A PI controller proved to have less overshoot and had less settling time than the PID controller.
- ► Temperature was controlled using ladder logic where it would heat to the set point temperature and switch off.



E 50

40

30